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APPLICATION NO.	FILING DATE	FIRST NAMED INVENTOR	ATTORNEY DOCKET NO.	CONFIRMATION NO.
10/677,545	10/02/2003	Eric Chao Xu	ANDRPR/385/US	9559
2543 7590 07/30/2007 ALIX YALE & RISTAS LLP 750 MAIN STREET SUITE 1400 HARTFORD, CT 06103			EXAMINER CORDRAY, DENNIS R	
			ART UNIT 1731	PAPER NUMBER
			MAIL DATE 07/30/2007	DELIVERY MODE PAPER

Please find below and/or attached an Office communication concerning this application or proceeding.

The time period for reply, if any, is set in the attached communication.

**Office Action Summary**

Application No.

10/677,545

Applicant(s)

XU, ERIC CHAO

Examiner

Dennis Cordray

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-- The MAILING DATE of this communication appears on the cover sheet with the correspondence address --

**Period for Reply**

A SHORTENED STATUTORY PERIOD FOR REPLY IS SET TO EXPIRE 3 MONTH(S) OR THIRTY (30) DAYS, WHICHEVER IS LONGER, FROM THE MAILING DATE OF THIS COMMUNICATION.

- Extensions of time may be available under the provisions of 37 CFR 1.136(a). In no event, however, may a reply be timely filed after SIX (6) MONTHS from the mailing date of this communication.
- If NO period for reply is specified above, the maximum statutory period will apply and will expire SIX (6) MONTHS from the mailing date of this communication.
- Failure to reply within the set or extended period for reply will, by statute, cause the application to become ABANDONED (35 U.S.C. § 133). Any reply received by the Office later than three months after the mailing date of this communication, even if timely filed, may reduce any earned patent term adjustment. See 37 CFR 1.704(b).

**Status**

- 1) ☒ Responsive to communication(s) filed on 24 May 2007.
- 2a) ☐ This action is **FINAL**. 2b) ☒ This action is non-final.
- 3) ☐ Since this application is in condition for allowance except for formal matters, prosecution as to the merits is closed in accordance with the practice under *Ex parte Quayle*, 1935 C.D. 11, 453 O.G. 213.

**Disposition of Claims**

- 4) ☒ Claim(s) 1-16, 18-23, 28-34, 36-38 and 42-49 is/are pending in the application.
- 4a) Of the above claim(s) \_\_\_\_\_ is/are withdrawn from consideration.
- 5) ☐ Claim(s) \_\_\_\_\_ is/are allowed.
- 6) ☒ Claim(s) 1-16, 18-23, 28-34, 36-38 and 42-49 is/are rejected.
- 7) ☐ Claim(s) \_\_\_\_\_ is/are objected to.
- 8) ☐ Claim(s) \_\_\_\_\_ are subject to restriction and/or election requirement.

**Application Papers**

- 9) ☐ The specification is objected to by the Examiner.
- 10) ☐ The drawing(s) filed on \_\_\_\_\_ is/are: a) ☐ accepted or b) ☐ objected to by the Examiner.  
Applicant may not request that any objection to the drawing(s) be held in abeyance. See 37 CFR 1.85(a).  
Replacement drawing sheet(s) including the correction is required if the drawing(s) is objected to. See 37 CFR 1.121(d).
- 11) ☐ The oath or declaration is objected to by the Examiner. Note the attached Office Action or form PTO-152.

**Priority under 35 U.S.C. § 119**

- 12) ☐ Acknowledgment is made of a claim for foreign priority under 35 U.S.C. § 119(a)-(d) or (f).
- a) ☐ All b) ☐ Some \* c) ☐ None of:
1. ☐ Certified copies of the priority documents have been received.
  2. ☐ Certified copies of the priority documents have been received in Application No. \_\_\_\_\_.
  3. ☐ Copies of the certified copies of the priority documents have been received in this National Stage application from the International Bureau (PCT Rule 17.2(a)).

\* See the attached detailed Office action for a list of the certified copies not received.

**Attachment(s)**

- |  |   |
|--|---|
| 1) <input type="checkbox"/> Notice of References Cited (PTO-892)                     | 4) <input type="checkbox"/> Interview Summary (PTO-413)           |
| 2) <input type="checkbox"/> Notice of Draftsperson's Patent Drawing Review (PTO-948) | Paper No(s)/Mail Date. _____                                      |
| 3) <input type="checkbox"/> Information Disclosure Statement(s) (PTO/SB/08)          | 5) <input type="checkbox"/> Notice of Informal Patent Application |
| Paper No(s)/Mail Date _____  | 6) <input type="checkbox"/> Other: _____                          |

## **DETAILED ACTION**

### ***Response to Arguments***

Applicant's arguments, see p 18, filed 5/24/2007, with respect to the combination of Prusas and Haynes et al with respect to the teaching of two alkaline peroxide pretreatment steps have been fully considered and are persuasive. The rejections of Claims over Prusas in view of Haynes et al and further in view of Cannell et al and others have been withdrawn. However, upon further consideration, new grounds of rejection are made in view of a modified interpretation of the cited prior art. In the current rejections, Prusas et al is only used to teach what was generally known to one of ordinary skill in the art at the time of the invention.

Applicant's arguments, see pp 14-15 with respect to the rejection of Claims 20 and 21 under 35 U.S.C. 112, 1st paragraph have been fully considered but are not persuasive. The Specification recites on p 8, lines 9-11 that the "alkaline peroxide chemicals may be introduced immediately (from less than a few inches to a few feet) after the blow valve". While the broad limits overlap the new claim limitation, there is no support within the Specification for the specific limitation of less than three feet. The Specification fails to define what is meant by "a few feet" and no examples are provided wherein the chemicals are introduced within three feet after the blow valve. New or amended claims which introduce elements or limitations which are not supported by the as-filed disclosure violate the written description requirement. See, e.g., *In re Lukach*, 442 F.2d 967, 169 USPQ 795 (CCPA 1971) (subgenus range was not supported by

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generic disclosure and specific example within the subgenus range). The rejection is maintained.

With regard to the arguments against Cannell et al, pp 16-18, the reference was used to provide a general teaching of a typical BCTMP process generally known to those of ordinary skill in the art. The generally known process comprises multiple DTPA and alkaline peroxide impregnations prior to the main refining step as well as bleaching following the main refining step and prior to any other process steps. A post-refining bleaching tower as known in the art is disclosed in the instant Specification (p 10; lines 1-4) and claimed in amended Claim 42. The Examiner acknowledges that Cannell et al does not teach adding alkaline peroxide into the blow line. With regard to Cannell et al teaching sulfite impregnation, the referenced process flow diagram indicates sodium sulfite or hydrogen peroxide and caustic in the multistage impregnation step.

Applicant argues that Haynes et al does not disclose any AP pretreatment upstream of the refiner. An alkaline peroxide treatment of the pulp in the refiner or prior to the refiner is disclosed (col 12, lines 39-42, Fig. 2, items 260, 261 and 263). There is no disclosure of removing the alkaline peroxide prior to the refiner, thus the alkaline peroxide prevails through the refiner. With regard to the replacement of sodium hydroxide with magnesium hydroxide, Haynes et al states, "According to the present invention, a suitable buffer and substitute alkali for sodium hydroxide is magnesium hydroxide which can be in any amount greater than 0% to 100% of what would be a suitable quantity of sodium hydroxide, preferably between about 40% to 100%..." (col 6, lines 26-31). Thus, in some embodiments, more than half of the alkalinity arises from

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sodium hydroxide. The instant claims only recite a sodium hydroxide alkaline peroxide treatment, and Haynes et al discloses embodiments wherein the treatment solution comprises sodium hydroxide and alkaline peroxide, thus is a sodium hydroxide alkaline peroxide treatment.

***Claim Rejections - 35 USC § 103***

The following is a quotation of 35 U.S.C. 103(a) which forms the basis for all obviousness rejections set forth in this Office action:

(a) A patent may not be obtained though the invention is not identically disclosed or described as set forth in section 102 of this title, if the differences between the subject matter sought to be patented and the prior art are such that the subject matter as a whole would have been obvious at the time the invention was made to a person having ordinary skill in the art to which said subject matter pertains. Patentability shall not be negated by the manner in which the invention was made.

Claims 1-11, 18-23, 28-29, 36-39 and 42-49 are rejected under 35 U.S.C. 103(a) as being unpatentable over Haynes et al (U 6,743,332) in view of Cannell et al ("The Future of BCTMP", Pulp and Paper, May 2000, supplied by applicant) and further in view of Prusas (4,486,267).

Claims 1-4, 8, 18-19, 22-23, 28, 36-37 and 42-43: Haynes et al discloses a method of making bleached mechanical pulps comprising (Abs; col. 5, lines 36-46; col 11, lines 53-64; col 12, lines 1-12; Fig. 2, item 224; col 13, lines 31-36; col 14, line 45 to col 15, line 8, Example 1):

- feeding wood chips, or lignocellulosic material, into a pressure disk refiner (inherently or obviously at an inlet to the refiner);
- refining the pulp at a temperature between 85 and 160 °C at a pressure of about 11 to 40 psi (68.9 to 276 kPa);
- the pulp having a consistency of about 10% to 50%; and

- delivering a stream of refined (primary) pulp from the casing of the refiner to a blow while the primary pulp temperature is between 85 and 160 °C.

The pressure refiner has a superatmospheric casing to allow operation at elevated pressures. The feed is in the form of wood chips, thus has been previously refined. Multiple alkaline peroxide treatments of the pulp are disclosed, including treatment in the refiner or prior to the refiner (col 12, lines 39-53, Fig. 2, items 260, 261 and 263). In addition, a second alkaline peroxide (intermediate or blow line) solution is mixed with the stream of primary pulp within the intermediate (blow) line while the primary pulp temperature is between 85 and 160 °C (col. 5, lines 12-20 and 36-45; col. 8, lines 10-14, Fig. 2, item 262; col. 12, lines 49-53; col 15, lines 8-10, Example 1) to form a reaction mixture in the intermediate line (col. 5, lines 41-45). Haynes also discloses that the second addition of the alkaline peroxide (intermediate or blow line) solution can be added at vessels, cyclone cleaner, conveyors (Fig 2, blocks 218, 258, 226, 230) and all lines connected to such blocks, including after the primary refiner and prior to additional refining (Fig 2, item 262) (col 12, lines 42-62). The components of the bleaching liquor, including the alkaline component can be added concurrently or together as part of the bleaching liquor (col 5, lines 6-12). An inlet port is inherent or, at least, would have been obvious to one of ordinary skill in the art to allow for the addition of treatments. Including a blow valve for discharging the solution from the pressurized refiner into the blow line is also inherent or would also have been obvious. In some embodiments, the reacting mixture having a temperature between 85 and 160 °C is discharged into a retention vessel, such as a surge vessel or a further portion of the

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blow line after the addition and mixing, (col. 8, lines 10-14) and contact time in the lines and vessels is controlled (the reaction mixture is retained) to produce a bleached material (col 5, lines 12-20; col. 13, line 64 - col. 14, line 8).

Haynes et al does not disclose the following:

- Feeding a lignocellulosic material into a first press,
- Pressing the lignocellulosic material,
- Discharging the material from the first press,
- Impregnating the material with a sodium hydroxide alkaline peroxide solution and maintaining the impregnation for a reaction time.

Cannell et al teaches a typical BCTMP (bleached chemical thermomechanical pulp) flow process (Fig 2, bottom of page 9 of provided article) that includes a multistage impregnation with an aqueous solution of DTPA, hydrogen peroxide and caustic, a primary refining stage, and a bleaching stage following the primary refining stage prior to any other process stages. Cannell thus teaches that pre-refining treatment with caustic and peroxide as well as post refining bleaching are typical steps practiced in the art.

Prusas discloses an alkaline peroxide mechanical pulping process comprising the steps of pretreating a lignocellulosic material by feeding a lignocellulosic material into a first press (col. 5, lines 5-12), pressing the lignocellulosic material (col. 5, lines 13-19); discharging the lignocellulosic material from the first press (col. 5, lines 13-19), impregnating the lignocellulosic material discharged from the first press with a first alkaline peroxide pretreatment solution (col. 5, lines 20-44) and maintaining the

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impregnation for a first reaction time (col. 5, line 65 - col. 6, line 7). Impregnation of lignocellulosic material by pressing and then allowing an impregnating solution to be drawn into the material upon release of pressure in the manner disclosed by Prusas is generally known in the art.

The art of Haynes et al, Cannell et al, Prusas and the instant invention is analogous as pertaining to the art of producing bleached CTMP pulps. At the time of the invention, it would have been obvious to a person of ordinary skill in the art to pretreat the lignocellulosic material by impregnation with an alkaline peroxide solution using the claimed steps in the pulping process of Haynes et al in view of Cannell et al and further in view of Prusas as a generally known treatment of lignocellulosic material. Including a multistage impregnation pretreatment of the lignocellulosic material would have been obvious as a typical process sequence, as taught by Cannell et al. Using the same sequence of steps for the second impregnation as for the first would also have been obvious as a generally known process.

Claim 5: Haynes et al discloses that the step of mixing (Fig. 3, item 336) is immediately followed by introducing the mixture into a separator (Fig. 3, item 338) and the separated pulp is then discharged into a retention vessel (Fig. 3, item 348).

Claim 6-7, 20-21 and 38: Haynes et al is not specific as to where in the blow line the alkaline peroxide treatment is added, but discloses addition of bleaching chemicals in the lines (Fig 2, 262) between the first refiner and process equipment following the first refiner. Absent data showing special properties derived from a particular point of addition in the blow line as compared to other locations in the line, it would have been



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obvious to one of ordinary skill in the art to add the treatment at any location within the line, including near the blow valve or cyclone separator, as a functionally equivalent option.

Claims 9 and 10: Haynes et al does not disclose altering the temperature or consistency of the mixed pulp and alkaline peroxide. Absent data showing special properties derived from a particular temperatures and consistencies, it would have been obvious to one of ordinary skill in the art to maintain the temperature and consistency achieved in the refining for further refining or processing.

Claims 11 and 29: Haynes et al discloses that the bleaching liquor comprises chelating agents and/or silicates to stabilize the peroxide (col 9, line 56 to col 10, line 11). Keeping the peroxide solution at lower temperatures prior to treating the pulp would have been obvious to minimize the peroxide decomposition reactions.

Claims 44-49: Haynes et al, Prusas and Cannell et al do not disclose the relative amounts of sodium hydroxide alkaline peroxide solution added prior to refining versus post refining. The amount of bleaching chemical added to a pulp is a known result-effective variable related to the whiteness of the pulp. It would have been obvious to one of ordinary skill in the art at the time of the invention to determine, through routine experimentation, the optimum amounts of bleaching chemicals added at the various points in the process to obtain the desired whiteness and to obtain the claimed amounts. Alternatively, it would have been obvious to add similar amounts of bleaching liquor at each addition point before, during and after the refining step.

Claims 12-16 and 30-34 are rejected under 35 U.S.C. 103(a) as being unpatentable over Haynes et al, Prusas, and Cannell et al, as applied to claims 1-2 and 21-22 above, and further in view of Textor ( 3,023,140), Sandstrom et al (4,270,976), and Xu (Xu, Eric C., "Chemical Treatment in Mechanical Pulping - Part 3; Pulp Yield and Chemical Pretreatment", 1998 Pulping Conference, TAPPI Proceedings, pp. 391-402, supplied by applicant).

The transition term "contains" is open-ended and must include at least the amounts of the reagents recited, but does not preclude other reagents or larger amounts of reagent. Therefore, the Examiner has considered the amounts claimed to indicate a lower end of a range of concentrations for each reagent.

Claims 12-16: Haynes et al discloses an acceptable alkalinity to hydrogen peroxide ratio in the bleaching liquor of about 0.25 to about 3 on a weight basis (col. 7, lines 2-4). The alkalinity limitation endpoints of claims 12-16 all fall within this range. Haynes also discloses adding a chelating agent, such as DTPA, in an amount of up to 10% by weight (col. 7, lines 7-18), which encompasses the claimed limitation endpoints of claims 12-16. Haynes further discloses use of sodium silicate up to about 10% by weight (col. 7, lines 32-33), which encompasses the limitation endpoints of claims 12-16. Additionally, Haynes et al discloses a suitable amount of hydrogen peroxide is 0.45% by weight to 9% by weight (10 to about 200 pounds per ton) based on dry pulp (col. 6, lines 62-64), which encompasses the limitation endpoints for claims 12-16, and also discloses a residual peroxide level of greater than 0.7% (col. 10, line 67 to col. 11, line 2), which also encompasses the limitation endpoints for claims 12-16.

Haynes et al does not disclose expressly the use of magnesium sulfate or residual alkalinity in the impregnating solution.

Textor discloses an alkaline peroxide mechanical pulping process (col. 3, line 73 to col. 4, line 1) in which magnesium sulfate is used to stabilize the peroxide bleach liquor (col. 3, lines 8-9). Textor discloses expressly a concentration of .05% magnesium sulfate (col. 3, lines 4-6), which contains one specific point within the claimed range of the 1st impregnation solutions of claims 14, 15, and 16, and within the 2nd impregnation fluids of claims 15 and 16.

Sandstrom et al discloses an alkaline peroxide mechanical pulping process (col. 1, lines 9-20) in which magnesium sulfate is added to the bleach liquor in an amount of 0.1 to 0.5% of the dry lignocellulosic material (col. 3, lines 4-13), which encompasses the claimed limitation endpoints of the second impregnation solutions of claims 12 and 13, and the intermediate line solutions of claims 12, 13, and 14. The range disclosed by Sandstrom et al also contains two specific points within the claimed ranges of claim 14, 1st and 2nd impregnation solutions, claim 15, 1st and 2nd impregnation solutions and intermediate line solution, and claim 16, 1st and 2nd impregnation solutions.

Xu discloses a total alkalinity residual of 0.1% in a 1st impregnation stage and 1.3% in a 2nd impregnation stage (p. 397, Table II, rows 4 and 7), and a total "total alkalinity" residual of up to 3.1 (p. 398, Table III, row 17), which contains at least one specific point within the claimed ranges of claims 12-15, intermediate line solutions.

The art of Haynes et al, Prusas, Cannell et al, Textor, Sandstrom et al, Xu and the instant invention is analogous as pertaining to the art of producing bleached CTMP

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pulps. Absent data showing special properties derived from the particular claimed compositions as compared to broader disclosures in the prior art, it would have been obvious to one of ordinary skill in the art to use magnesium sulfate as described by Textor and Sandstrom et al as a functionally equivalent option and to optimize the amount of magnesium sulfate to obtain the most efficient use of the reagent as a stabilizer for the peroxide solution (Textor, col. 3, lines 8-9). The amount of peroxide is a known result effective variable and it would have been within the capability of one of ordinary skill in the art to optimize the concentration of peroxide, and thereby the sodium hydroxide and stabilizer, in the bleaching liquors to provide the greatest whitening effect. Obtaining the claimed residual alkaline and peroxide would also result from the optimization.

Claims 30-34 are treated similarly to Claims 12-16.

### ***Conclusion***

Any inquiry concerning this communication or earlier communications from the examiner should be directed to Dennis Cordray whose telephone number is 571-272-8244. The examiner can normally be reached on M - F, 7:30 -4:00 PM.


If attempts to reach the examiner by telephone are unsuccessful, the examiner's supervisor, Steven Griffin can be reached on 571-272-1189. The fax phone number for the organization where this application or proceeding is assigned is 571-273-8300.

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Information regarding the status of an application may be obtained from the Patent Application Information Retrieval (PAIR) system. Status information for published applications may be obtained from either Private PAIR or Public PAIR. Status information for unpublished applications is available through Private PAIR only. For more information about the PAIR system, see <http://pair-direct.uspto.gov>. Should you have questions on access to the Private PAIR system, contact the Electronic Business Center (EBC) at 866-217-9197 (toll-free). If you would like assistance from a USPTO Customer Service Representative or access to the automated information system, call 800-786-9199 (IN USA OR CANADA) or 571-272-1000.

*QRe*

DRC

  
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